



CO₂ and H₂S Absorption in Tofu Liquid Waste Biogas using Packed Bed Scrubber with Variation of MEA Concentration and Flow Rate

Aan Adeputra¹, Leila Kalsum^{2*} & Abu Hasan²

¹Applied Master of Renewable Energy Engineering, Politeknik Negeri Sriwijaya, Palembang, Indonesia

²Department of Chemical Engineering, Politeknik Negeri Sriwijaya, Palembang, Indonesia

Email address:

leila_k@polsri.ac.id

*Corresponding author

To cite this article:

Putra, A. A., Kalsum, L., & Hasan, A. CO₂ and H₂S Absorption in Tofu Liquid Waste Biogas using Packed Bed Scrubber with Variation of MEA Concentration and Flow Rate. *International Journal of Research in Vocational Studies (IJRVOCAS)*, 3(2), 23–28.

<https://doi.org/10.53893/ijrvocas.v3i2.204>

Received: 07 10, 2023; **Accepted:** 07 29, 2023; **Published:** 08 25, 2023

Abstract: Biogas technology has become an alternative fuel that is often used in Indonesia. One of the raw materials for biogas that has the potential and is easy to obtain is waste from the tofu industry. Liquid waste still contains a lot of organic elements. The organic materials contained in the exhaust of the tofu industry are generally very high. The gases commonly found in tofu waste are nitrogen gas (N₂), oxygen (O₂), hydrogen sulfide (H₂S), ammonia (NH₃), carbon dioxide (CO₂) and methane (CH₄). These gases come from the decomposition of organic materials contained in wastewater. So that biogas produced from tofu liquid waste still contains CO₂ and H₂S gases which are quite high. Therefore, in this study the process of purification or refining of biogas products will be carried out using the absorption method through an absorber column using monoethanolamine (MEA) solution as a chemical absorbent through a 8 mm packed bed scrubber. The results showed that the best biogas flow rate in the purification process, which produced the highest CH₄ concentration of 95.12% was 40% MEA concentration and 0.8 L/min flow rate. The effect of MEA concentration on biogas purification causes the concentration of CO₂ and H₂S in the purified biogas to decrease as the MEA concentration increases. The best combination of 0.8 L/min biogas flow rate and 10 mm packing area reduces CO₂ and H₂S concentrations to 1.88% and 0 ppm.

Keywords: Absorption, Biogas, MEA, Tofu Liquid Waste

1. Introduction

Biogas technology has become an alternative fuel that is often used in Indonesia [1]. Biogas is a renewable non-fossil fuel which can be used as an alternative to bioenergy. The biogas product consists of (CH₄) methane 50 – 70%, (CO₂) carbon dioxide 25 – 45%, and small amounts of (H₂) hydrogen, (N₂) nitrogen, and (H₂S) hydrogen sulfide [2]. Methane gas (CH₄) is the main component of biogas which is used as a fuel with many benefits. Biogas has a high calorific value, which is around 4800 to 6700 kcal/m³, while pure methane gas contains an energy of 8900 Kcal/m³ [3].

Biogas can be produced from a mixture of livestock manure such as cattle and liquid organic waste in industries

such as tofu [4]. Apart from the fact that this material contains the elements carbon (C), hydrogen (H) and nitrogen (N), waste from the tofu industry is waste that has the potential to be reused because of the large number of tofu industries in Indonesia which have reached approximately 84,000 business units with production capacity of more than 2.56 million tons per year with the production of liquid waste of 20 million m³/year [5]. The relatively high agricultural and livestock sector is also the reason why these resources must be processed in such a way as to produce more useful products [6]. The methane gas content produced from tofu industrial waste also varies. Adisasmito in his research, produced 56%

methane gas and 43% carbon dioxide gas [7]. While Harihastuti's research, the biogas digester produced a product containing around 46% methane gas, 30% carbon dioxide gas, and other gases, including ammonia, hydrogen sulfide and other gases [8],[9].

Furthermore, this biogas product will undergo a purification process from the content of acidic gases such as CO₂ and H₂S. CO₂ and H₂S elements in biogas are very detrimental to equipment made of metal because they are corrosive. Carbon dioxide (CO₂) is a dangerous gas that reduces the density and reduces the heating value of biogas but is not as toxic and corrosive as H₂S. This element is also harmful to the environment and is detrimental to metal parts of engines pumps, compressors, gas storage tanks, valves and reduces the life of equipment processes [10],[11],[12]. The amount of CO₂ and H₂S is expected to be below 1% in the presence of biogas. These conditions can be obtained through the biogas purification process. The biogas purification process to reduce CO₂ and H₂S gas can be carried out through an absorption process [13],[14]. Materials that can be used to absorb monoethanolamine (MEA). The MEA compound is a primary amine compound, in which the compound contains only 1 amine group. The amine solution can physically and chemically absorb CO₂ and H₂S gas, so that the mass transfer from the gas phase to the liquid phase of the two gases increases due to the chemical reaction [15],[16].

Based on information regarding the previous biogas

purification process, this research will be carried out by purifying the biogas product using the absorption method through an absorber column with a solution of the chemical monoethanolamine (MEA) as a chemical absorbent which is injected from the top of the absorber column, then contact between the biogas and the MEA solution occurs along the packing column to the bottom of the column [17].

2. Research Method

2.1. Preparation

The raw material in the form of tofu industrial waste is the basic material used in this experiment. Prior to the biogas production process, the tofu industrial wastewater is subjected to biological and chemical analysis including the degree of acidity of pH, COD, and TSS.

2.2. Biogas

In research on the process of forming biogas in the biodigester. Experimental techniques refer to research [18], [19]. As a source of fuel, tofu liquid waste and cow dung starter are used in mixed variations. The temperature and pH of the biodigester were monitored and recorded for 30 days during the fermentation process [20].

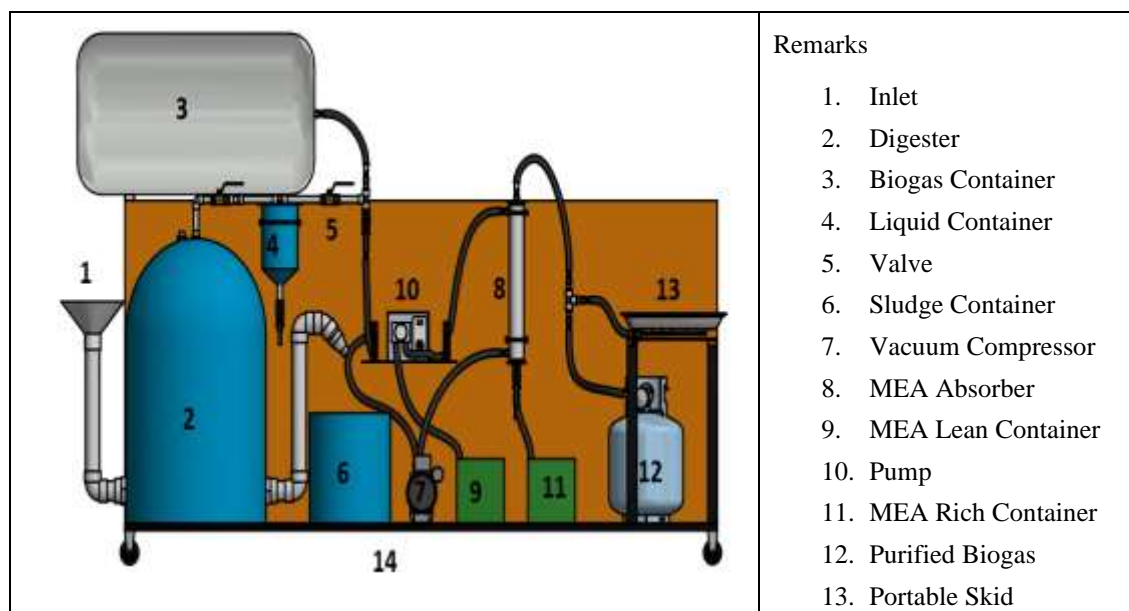


Figure 1. Biodigester and Absorber Unit

2.2. Purification

The biogas purification method is carried out by absorption technique, it has good absorption power for the biogas purification process. The absorbent used is MEA solution which has a very high degree of selectivity to CO₂.

Biogas purification has an optimum time on the 20th day [21].

The power supply for the MEA pump and vacuum compressor is ensured that it is connected to a power source. Every valve from the biogas reservoir, absorber and MEA pump is ensured to be open before turning on the MEA pump. The MEA pump is turned on to flow MEA through the top of the absorber by pressing the ON button for the MEA pump on

the control. panel. The MEA solution is allowed to circulate through the top of the absorber for 30 seconds. The biogas flow rate control valve into the absorber is opened and the vacuum compressor is turned on by pressing the ON button. by varying the research 0.2 L/min, 0.4 L/min, 0.6 L/min, and 0.8 L/min. After that, the biogas that has been purified in the absorber column is accommodated in a biogas storage tube. The results of the purification process were analyzed using a Multi Gas Detector Analyzer to determine the concentrations of CH₄, CO₂ and H₂S.

3. Result and Discussion

3.1. Characterization of Tofu Liquid Waste

Biomass characteristics such as tofu liquid waste have a high content of organic compounds such as proteins, fats and carbohydrates. So, at this stage, tofu waste analysis is carried out to determine the content of organic matter through several important organic physical and organic chemical parameters, Physical characteristics such as turbidity, temperature, solids, and turbidity, as well as organic chemical parameters, are the types of metrics that are utilized to demonstrate the characteristics of the wastewater produced by the tofu industry. Table 1 shows the organic content measured in terms of BOD, COD, total nitrogen, and pH values.

Tofu wastewater has a temperature of 35°C. This quantity can be utilized as raw material for biogas production, but it is high if it goes directly into water that is warm. This is since

the temperature that must be maintained for aquatic organisms to survive in tropical waters ranges between (25-32) °C.

The total soluble solids concentration (TSS) of the raw material that was generated is 1938 mg/L, which is a somewhat high value in comparison to the quality requirement of 400 mg/L. A significant amount of TSS is present in the liquid excrement. The color of the wastewater, which is murky, is an indication that the excess TSS concentration value is too high; this coloration corresponds to a yield of 50.2cp.

The organic chemical content of COD results in a value that is still within the range of 11105 mg/L from 11200 mg/L, while for a BOD value of 5652 mg/L, total nitrogen is 268 mg/l higher than the literature 5500 mg/L and 200mg/L. Additionally, the resulting pH of 3.5 does not enter the quality standard range, which is 5-9 [22].

Because of the high concentration of organic compounds (COD and BOD), the oxygen levels in the water will drop, which will be detrimental to aquatic animals like fish. Because of the high nitrogen content, there is also an offensive odor due to the presence of ammonia gas. The water's quality will suffer as a result, as will the amount of sunlight that can reach aquatic plants; without adequate light, these plants would be unable to carry out photosynthesis correctly. People have a greater risk of developing skin ailments and stomach discomfort when they utilize the water for day-to-day activities. For the liquid waste from tofu used in this study to possess sufficient organic matter to enable the production of biogas [23].

Table 1. Tofu Liquid Waste Analysis Result

Parameters	Unit	Method	Result
Physical Properties			
Temperatur	°C	SNI 6989.23-2005	35
Total Suspended Solids (TSS)	mg/L	Gravimetri	1938
Turbidity	cp	Viskometer	50.2
Chemical Properties			
COD	mg/L	Spectrophotometri	11105
BOD	mg/L	Winkler	5652
Nitrogen Total	g/L	Spectrophotometri	268
pH	-	SNI 6968.11-2019	3.62

*The data source is processed from Balai Besar Laboratorium Kesehatan Palembang

3.2. Biogas Composition before Gasification

The composition of the biogas produced depends on the organic source materials and the parameters established during the anaerobic degradation process. [21]. Figure 2 shows the initial content of the biogas produced as a result of the fermentation process that took place in the biodigester for a period of thirty days to produce high levels of CO₂ and H₂S gases. The CO₂ concentration in the biogas was 10.12% on day 30, whereas the H₂S concentration was 156% on the same day. The absence of an absorption mechanism is the reason for the high levels of CO₂ and H₂S that can be found in biogas.

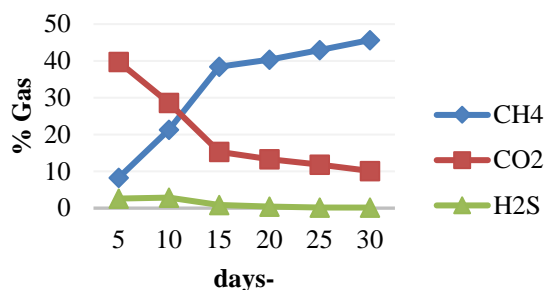
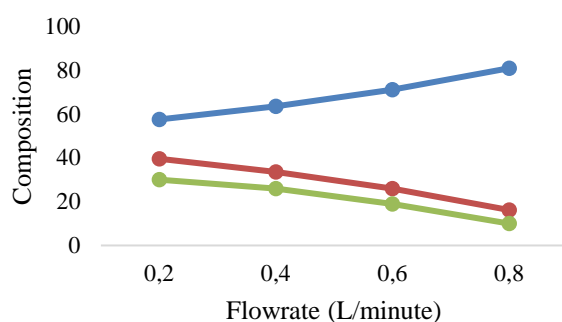
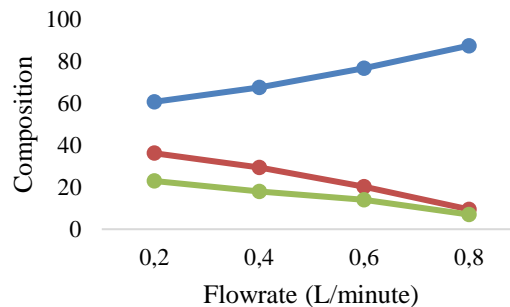


Figure 2. Biogas Composition Before Purification

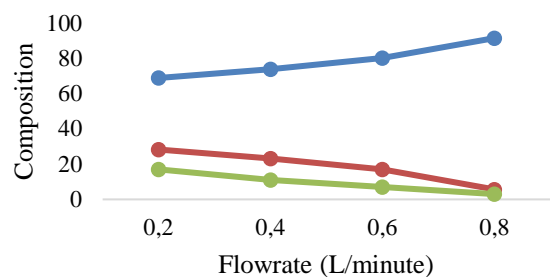
Therefore, with the expectation of lowering CO₂ and H₂S levels while boosting CH₄ content in biogas, researchers will



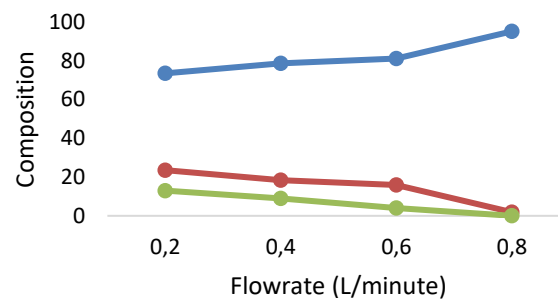
(a)



(b)



(c)



(d)

—●— CH₄ (%) —●— CO₂ (%) —●— H₂S (ppm)

Figure 3. Biogas Composition after Purification with MEA Concentration of (a) 10%, (b) 20%, (c) 30%, and (d) 40%

The pattern that can be seen in Figure 3 is that the amount of CH₄ that is found in biogas after it has been filtered with MEA continues to rise. After purification with MEA, the quantity of CH₄ in the biogas grew to 80.82%; 87.54%; 91.34%; and 95.12% at a MEA flow rate of 0.8 L/min with a MEA concentration of 10%, 20%, 30%, and 40% correspondingly. Prior to purification, the CH₄ content in the biogas was 45.67%. This suggests that the MEA content tends to rise with increasing MEA concentrations that are employed. In comparison to the other concentrations, the concentration of 40% generates the highest CH₄ content, which comes out to be 95.12%. The same is true for the MEA flow rate that is being

used; the longer the MEA is flowed, the higher the CH₄ content will be. This can be observed in one of the samples that was used when the MEA concentration was 10%, where the CH₄ composition at a flow rate of 0.2 minutes was lower than the CH₄ composition that was utilized when the flow rate was 0.8 minutes. The quantity of CH₄ that is created is inversely proportional to the quality of the biogas produced.

3.3. Biogas Composition after Purification

After the purification process is carried out, the H₂S and CO₂ content in the purified biogas is checked again. Checks are carried out every time the use of variations in MEA concentration and variations in MEA flow rate used in the absorption process. Figure 3 shows the relationship between H₂S and CO₂ content after the purification process and MEA absorption flow rate at each MEA concentration.

utilized; the longer the MEA is flowed, the higher the CH₄ content will be. This can be observed in one of the samples that was used when the MEA concentration was 10%, where the CH₄ composition at a flow rate of 0.2 minutes was lower than the CH₄ composition that was utilized when the flow rate was 0.8 minutes. The quantity of CH₄ that is created is inversely proportional to the quality of the biogas produced.

As can be seen from Figure 3a through 3d, the composition of CO₂ tends to become decreased with increasing MEA concentrations. The composition of CO₂ was 10.12% before it was purified, but after it was purified at 0.8 L/minute with a concentration of 40% MEA, it produced 1.88% CO₂, which is

a substantial reduction from the original value. The quality of the biogas produced is directly proportional to the amount of CO₂ that is contained within it. Because the CO₂ content in biogas will lower the heating value of the fuel, which is related to the nature of CO₂ as a by-product of the combustion process; specifically, CO₂ is a substance that does not burn anymore [26]. It is also possible to see, as a result of looking at Figure 3 a-d, that the reduction in CO₂ content is significantly more substantial the more concentrated the concentration that was employed. At flow rates ranging from 0.6 L/minute to 0.8 L/minute, this phenomenon is observable at concentrations of 10%, 20%, 30%, and 40%, respectively. At these flow rates, there is a difference in the reduction of CO₂ composition by 9.72%; 10.77%; 11.26%; and 14.06%.

H₂S was found to be the final component to be discovered. It is imperative that the concentration of H₂S be decreased since it is detrimental to human health, particularly the sense of smell. This is since H₂S can produce a characteristically unpleasant stench. In addition to this, the removal of H₂S from biogas as part of the purification process will safeguard engine components from the corrosive effects of biogas [19]. The H₂S content in biogas, which had been as high as 156% before the purification process with MEA, was reduced to 0% at the MEA concentration. The purification procedure required a MEA concentration of 40% and a flow rate of 0.8 minutes. This suggests that there is no longer any H₂S present in the biogas that has been created.

4. Conclusion

The results showed that the best biogas flow rate in the purification process produced the highest CH₄ concentration of 95.12% was 40% MEA concentration and 0.8 L/min flow rate. The effect of MEA concentration on biogas purification causes the concentration of H₂S in purified biogas to decrease with increasing MEA concentration. The best combination of biogas flow rate of 1 L/min and packed bed scrubber of 8 mm reduces CO₂ and H₂S concentration to 1.88% and 0 ppm. This is because the slow flow rate will cause the contact time between biogas and MEA to be longer and the contact area to be wider; therefore, more impurities will be absorbed and this in turn will lead to higher CH₄ yields.

Acknowledgements

The authors gratefully acknowledged Renewable Energy Engineering Department and Politeknik Negeri Sriwijaya.

References

- [1] Yahya, Y. (2017). *Produksi biogas dari campuran kotoran ayam, kotoran sapi, dan rumput gajah mini* (Pennisetum purpureum cv. Mott) dengan Sistem Batch.
- [2] Purba, E., & Barutu, C. N. R. 2021. The CO₂ Gas Absorption in Biogas Using Absorber Bubble Column with Variation of NaOH Absorbent Concentration and Sparger Forms. Indonesian Journal of Chemical Science, 10(1), 68-74.
- [3] Kristyan, E. G., Pratiwi, Y. R., & Putra, H. S. 2021. *Rancang Bangun Biogas Limbah Tahu Skala Rumah Tangga*. Journal of Science Nusantara, 1(2), 24-29.
- [4] Maryani, S. (2016). *Potensi Campuran Sampah Sayuran Dan Kotoran Sapi Sebagai Penghasil Biogas (Doctoral dissertation, Universitas Islam Negeri Maulana Malik Ibrahim)*.
- [5] Muzakki, J. A. (2021). *Pengaruh Penambahan Bioaktivator Em-4 Terhadap Produksi Biogas Dari Limbah Cair Industri Tahu*. Cermin: Jurnal Penelitian, 5(2), 362-372.
- [6] Bare, Y., Mago, O. Y. T., & Misa, A. (2022). *Pengaruh Campuran Limbah Tahu Dan Kotoran Sapi Terhadap Produksi Biogas*. Biopendix: Jurnal Biologi, Pendidikan Dan Terapan, 9(1), 10-18.
- [7] Adisasmto, S., Rasrendra, C. B., Chandra, H., & Gunartono, M. A. (2018). Anaerobic reactor for Indonesian tofu wastewater treatment. International Journal of Engineering & Technology, 7(3), 30-32.
- [8] Clinton, D., & Herlina, N. (2015). *Pengaruh Waktu Fermentasi dan Komposisi Limbah Kulit Buah Aren (Arenga pinnata) dengan Starter Kotoran Sapi Terhadap Biogas yang Dihasilkan*. Jurnal Teknik Kimia USU, 4(3).
- [9] Fatin, M. H., Husaini, A., & Kalsum, L. (2021). Effect of Adding Palm Oil Mill Effluent (POME) and Slurry on Biogas From Cow Manure to Produced Methane Gas BT - Proceedings of the 4th Forum in Research, Science, and Technology (FIRST-T1-T2-2020). 7, 75-80.
- [10] Hidayat, T., Yerizam, M., Hasan, A., & Rusdianasari. (2021). Modification of Fuel Input on Oil Fuel Electric Generator to Gas Fuel Engine. IOP Conference Series: Earth and Environmental Science, 709(1).
- [11] A. Ahmad, D. Andrio, T. Y. Putra, and U. Seprizal. (2022) "Proses Purifikasi untuk Penyisihan Kandungan Hidrogen Sulfida dan Karbon Dioksida di Dalam Biogas Menggunakan Mono Etanol Amin (MEA)," Equilibrium Journal of Chemical Engineering, vol. 5, no. 2, pp. 103-110
- [12] Nurhilal, M., Aji, G. M., Mesin, J. T., Cilacap, P. N., Elektronika, J. T., & Cilacap, P. N. (2020). *Pengaruh Komposisi Dan Waktu Fermentasi Campuran Limbah Industri Tahu Dan Kotoran Sapi Terhadap Kandungan Gas Methane Pada Pembangkit Biogas*. Jurnal Teknologi Terapan, 6(1).
- [13] Rajiman, V., Hairul, N. A. H., & Shariff, A. M. (2020). December. Effect of CO₂ concentration and liquid to gas ratio on CO₂ absorption from simulated biogas using monoethanolamine solution. In IOP Conference Series: Materials Science and Engineering (Vol. 991, No. 1, p. 012133). IOP Publishing.
- [14] Akkarawatkhoosith, N., Kaewchada, A., & Jaree, A. (2019). High-throughput CO₂ capture for biogas purification using monoethanolamine in a microtube contactor. Journal of the Taiwan Institute of Chemical Engineers, 98, 113-123.
- [15] Daiyan, I. N., Kalsum, L., & Bow, Y. (2020). Capturing CO₂ from Biogas by MEA (Monoethanolamine) using Packed Bed Scrubber. Jurnal Teknik Kimia dan Lingkungan, 4(2), 54-62.
- [16] Kulkarni, M. B., & Ghanegaonkar, P. M. (2019). Hydrogen sulfide removal from biogas using chemical absorption technique in packed column reactors. Global Journal of Environmental Science and Management, 5(2), 155-166.

- [17] Bow, Y., Kalsum, L., Hasan, A., Husaini, A., & Rusdianasari. (2021). The Purification of Biogas with Monoethanolamine (MEA) Solution Based on Biogas Flow Rate. *Proceedings of the 4th Forum in Research, Science, and Technology (FIRST-T1-T2-2020)*, 7, 1–5.
- [18] Ahmad, A., Bahrudin, B., Andrio, D., & Hamzah, A. The performance of a pilot-scale anaerobic hybrid bioreactor on palm oil mill effluent treatment. *Reaktor*, 19(3), 111-116.
- [19] Kalsum, L., & Hasan, A. (2022). The Effect of the Packing Flow Area and Biogas Flow Rate on Biogas Purification in Packed Bed Scrubber. *Journal of Ecological Engineering*, 23(11).
- [20] Sajaruddin, Kalsum, L., & Muchtar, Z. (2020). The Analysis of Biogas Fermentation Time from Cow Manure on Fixed Dome Biodigester Batch Systems. *Journal of Physics: Conference Series*, 1500(1).
- [21] Tetteh E., Amano KOA, Asante-Sackey D., Armah E. (2018). Optimasi Response Surface Potensi Biogas Pada Co-Digestion *Miscanthus Fuscus* dan Kotoran Sapi. *Jurnal Teknologi Internasional*, 9(5), 944-954.
- [22] Mufarida and O. D. Setiawan, (2020). Socialization of Tofu Liquid Waste Management (Whey Tofu) Becomes Biogas as Alternative Energy Reserves in the Framework of Creating an Environmentally Friendly Industry. *Kontribusi (Research Dissemination for Community Development)*, vol. 3, no. 2, p. 326, doi: 10.30587/kontribusi.v3i2.1452.
- [23] B. Budiyo & I. Syaichurrozi. (2020). A review: Biogas production from tofu liquid waste. *IOP Conference Series: Materials Science and Engineering*, vol. 845, no. 1, doi: 10.1088/1757-899X/845/1/012047
- [24] Sinaga, P. V. H., Suanggana, D., & Haryono, H. D. (2022). Analisis Produksi Biogas Sebagai Energi Alternatif Pada Kompor Biogas Menggunakan Campuran Kotoran Sapi Dan Ampas Tahu. *Jurnal Teknologi Terapan*, 8(1), 61-69.
- [25] Basri, A. K., Kadirman, K., & Jamaluddin, J. (2019). Rancang Bangun Reaktor Biogas Skala Rumah Tangga. *Jurnal Pendidikan Teknologi Pertanian*, 5(1), 79-84.
- [26] Kasikamphaiboon, P., Chungsiriporn, J., Bunyakan, C., & Wiyaratn, W. (2013). Simultaneous removal of CO₂ and H₂S using MEA solution in a packed column absorber for biogas upgrading. *Songklanakarin Journal of Science & Technology*, 35(6).